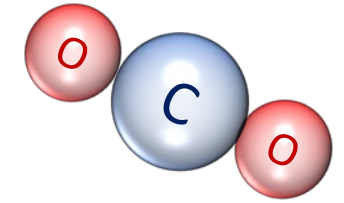
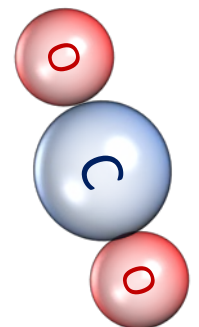
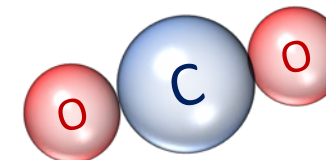
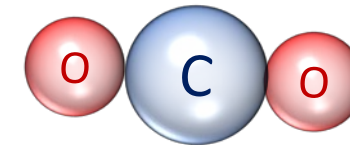
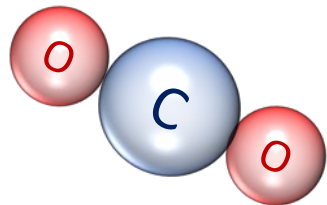


CO₂ Capture Systems and



Opportunities for Process Intensification

David C. Miller, Ph.D.
Senior Fellow
February 2020



Timeline of Carbon Capture Research

1997

NETL Carbon Capture Storage Program initiated with \$1mil

1992

First International Conference on Carbon Dioxide Removal (ICCDR-1)

2012

\$80-100/ton CO₂

Breakthrough CCS project at Air Products and Chemicals begins capturing CO₂ and sending to oilfield for EOR; Initial release of CCSI Toolset

2020

\$45/ton CO₂

Large scale pilot testing (10-25 Mwe) for 2nd gen tech

2007

10 year anniversary of CCS program, which has grown to \$100M

2014

Sask Power's Boundary Dam commissioned

1990

1995

2000

2005

2010

2015

2020

1993

DOE/MIT prioritize research needs for CO₂ capture and sequestration; first gen capture tech for PCC is aqueous amines

2003

DOE/NETL initiate Regional Carbon Sequestration Partnership (RCSP)

2011

DOE/NETL publishes Carbon Dioxide Capture and Storage RD&D Roadmap

2016

\$60/ton CO₂

2017

Petra Nova carbon emissions reduction system begins operation

2009

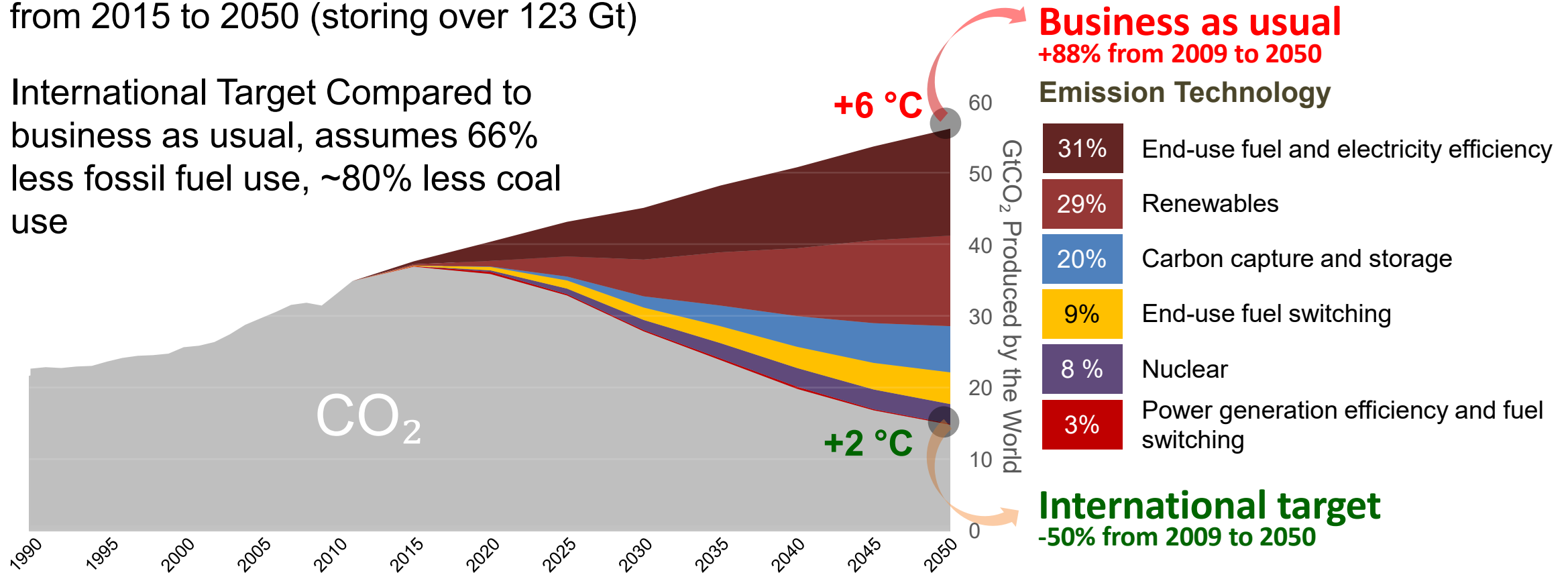
NETL announces 12 large-scale capture projects; First National Carbon Capture Center (NCCC) opens led by DOE/NETL and Southern Company Services

2025: 2nd gen tech target \$40/ton CO₂

2030: Transformational tech target \$30/ton CO₂

Need for CO₂ Capture

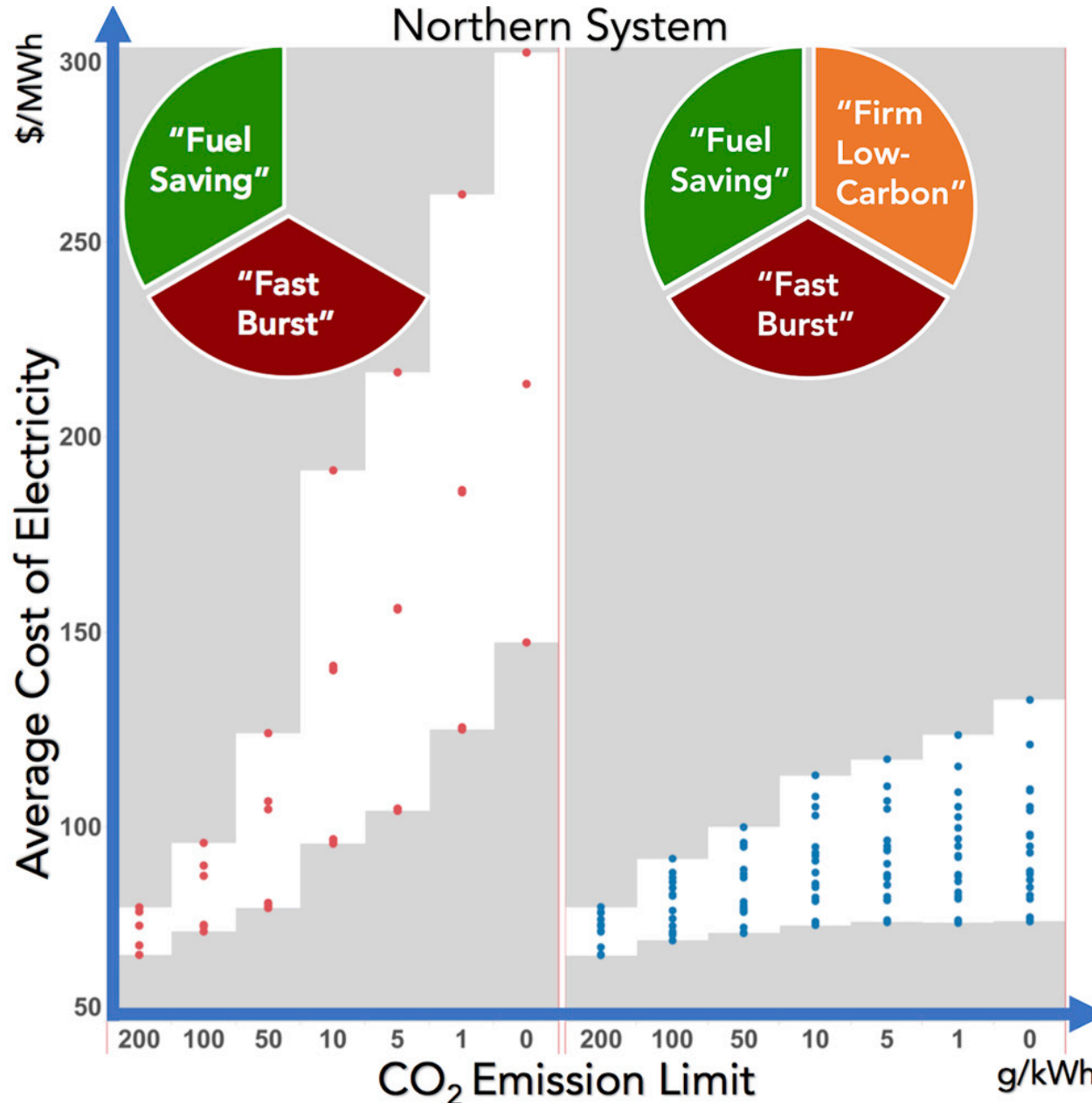
- CCS achieves 20% of cumulative reductions from 2015 to 2050 (storing over 123 Gt)
- International Target Compared to business as usual, assumes 66% less fossil fuel use, ~80% less coal use



- Limits to efficiency gains, fuel switching reductions and CCS only option for some industrial sectors

- Delaying or abandoning CCS would increase power sector compliance cost by 40+%

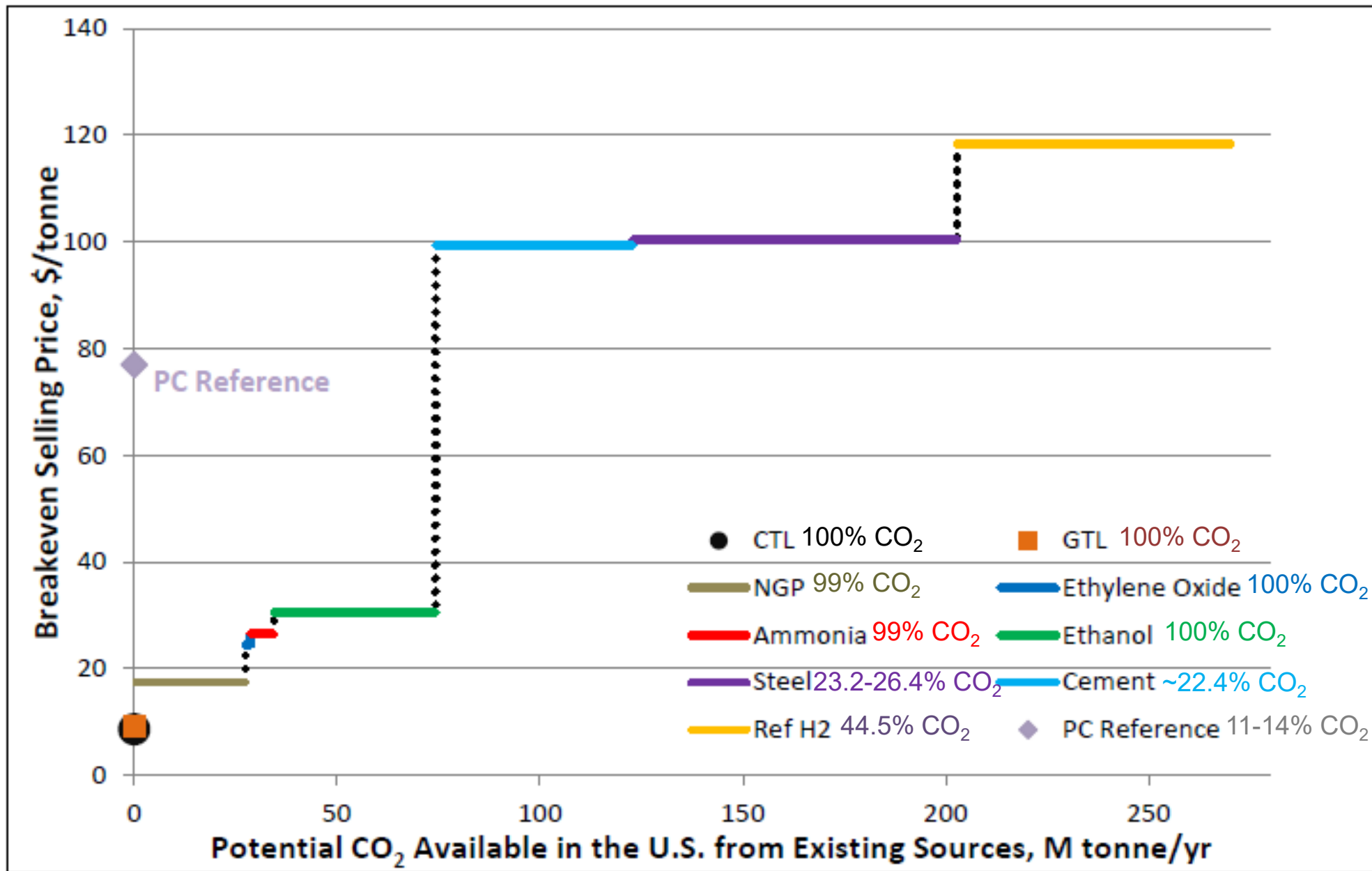
Dispatchable Power with Capture Lowers Costs



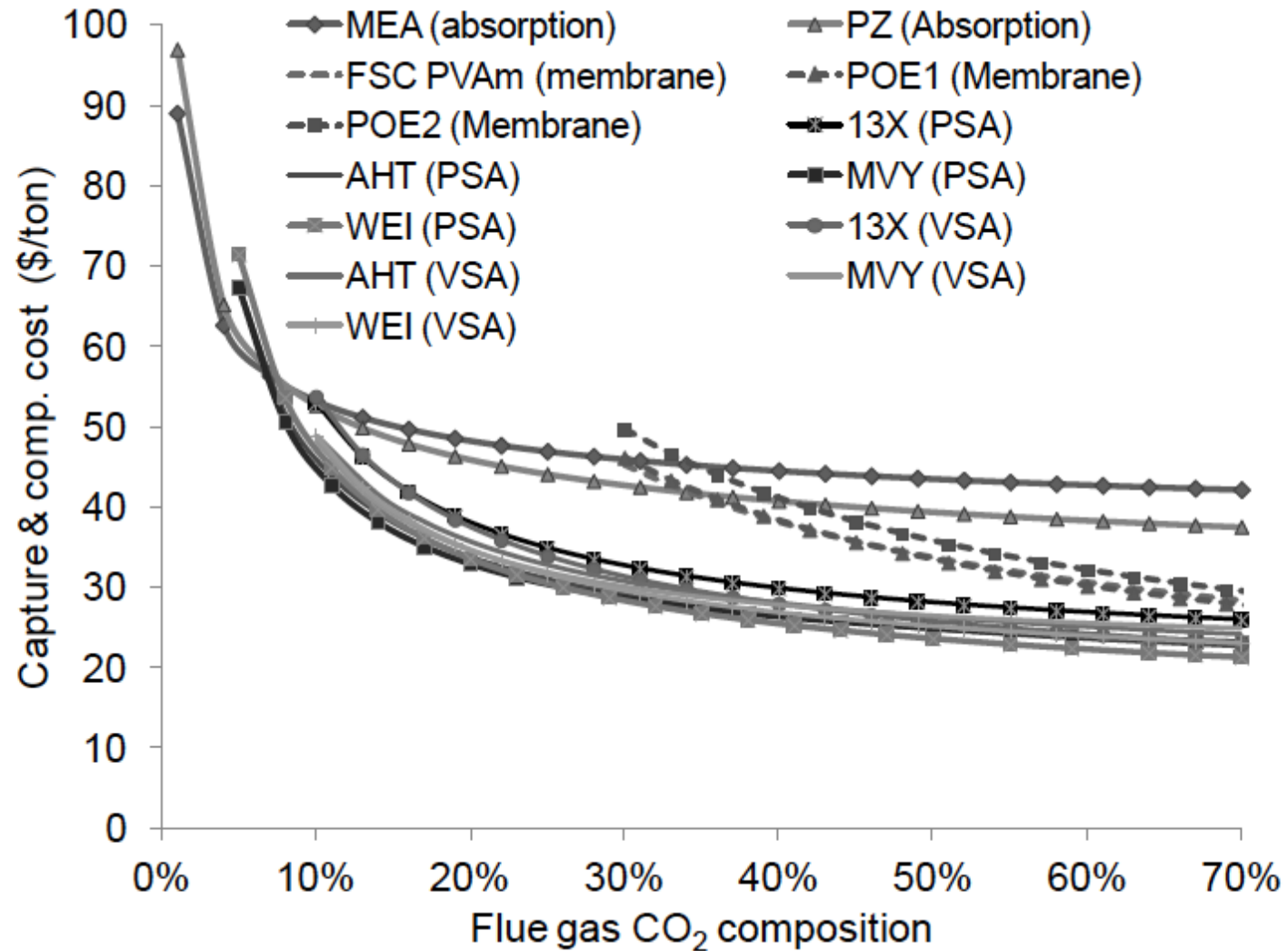
“Firm low-carbon” resources like CCS and nuclear lower the cost of deep decarbonization by 10-62%

Sepulveda, et al., Joule (2018)

<https://doi.org/10.1016/j.joule.2018.08.006>

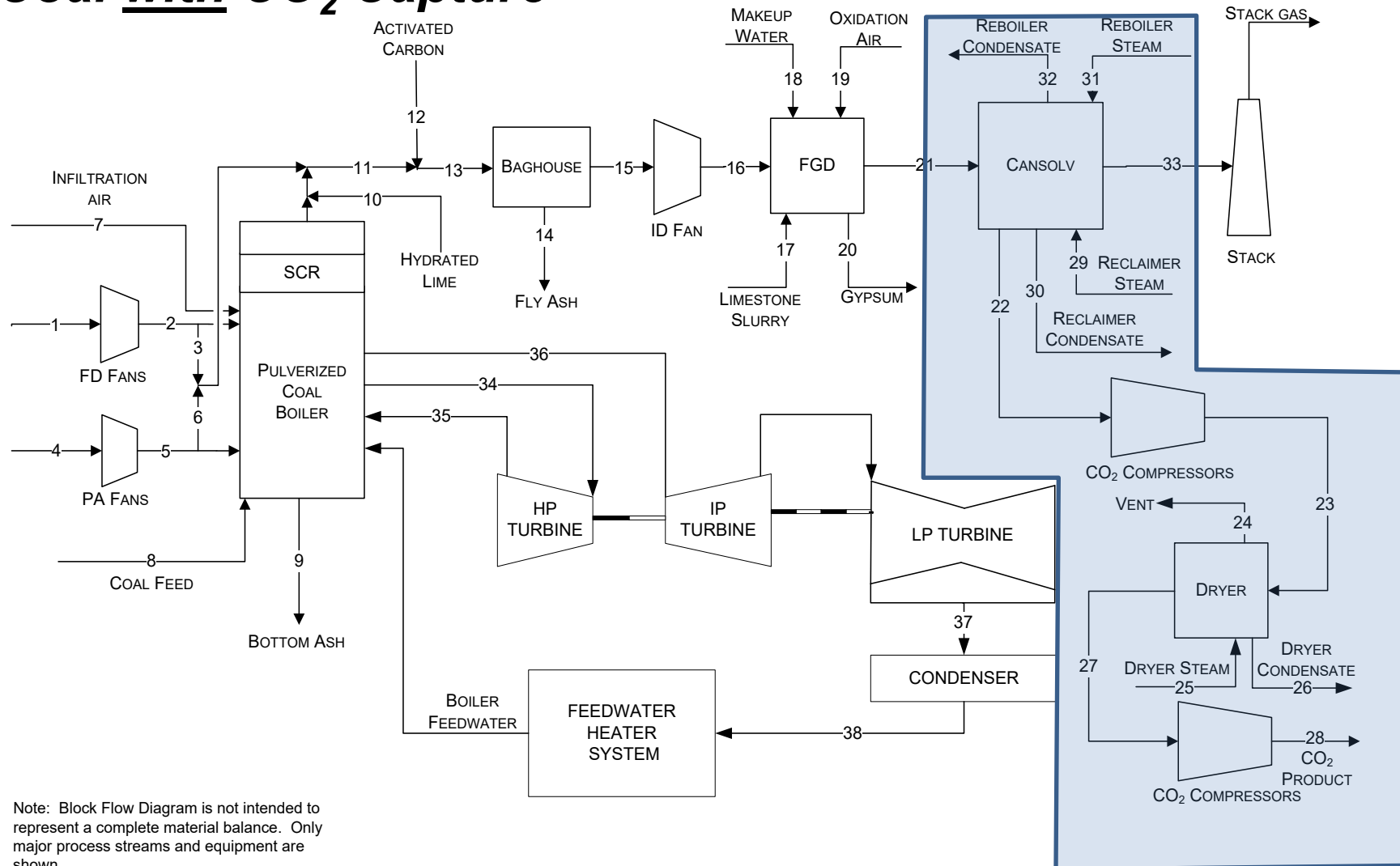


Cost Variability for Technology & CO₂ Concentration



Supercritical Pulverized Coal Power Plant

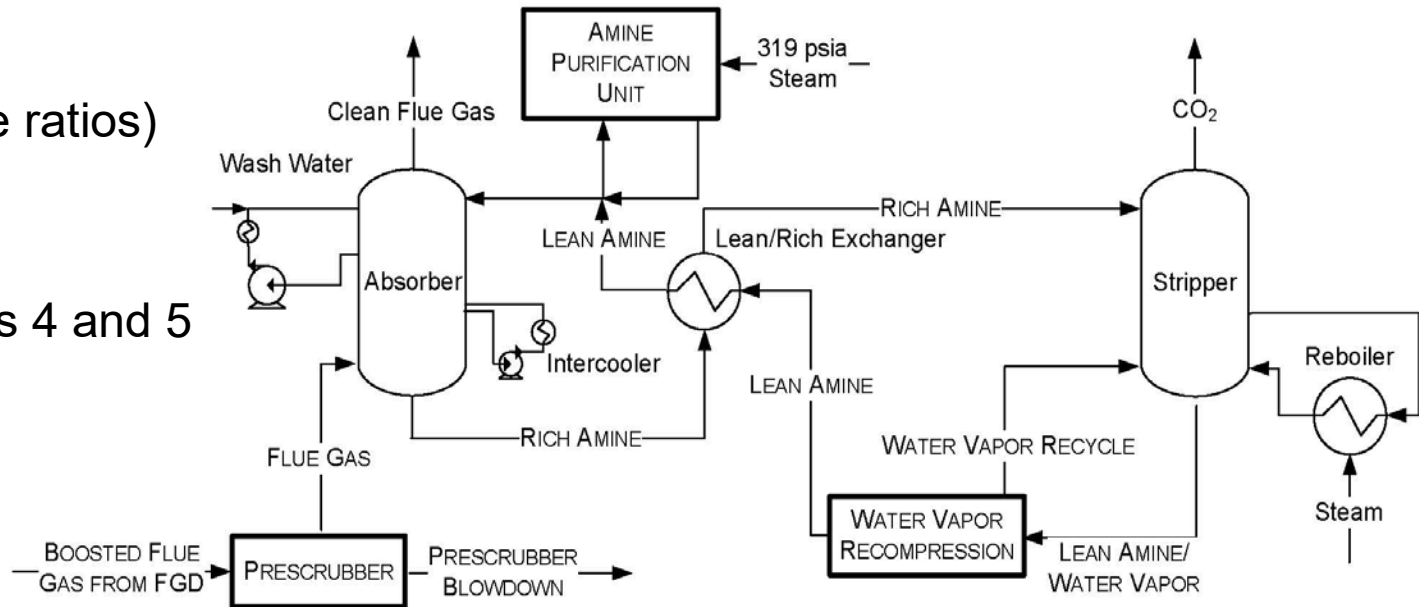
Conventional Coal with CO₂ Capture



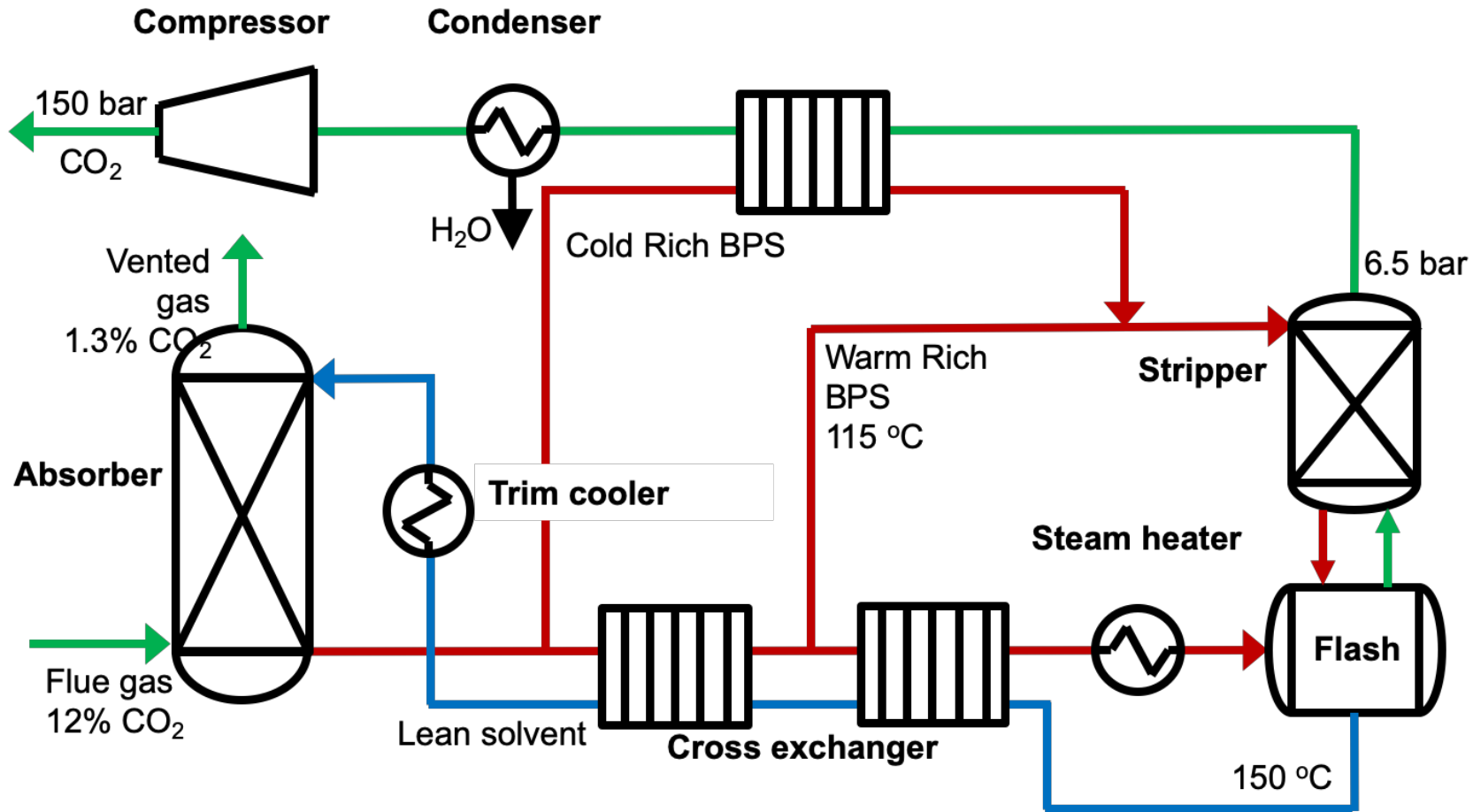
Note: Block Flow Diagram is not intended to represent a complete material balance. Only major process streams and equipment are shown.

Supercritical Pulverized Coal Power Plant

- Pre-treatment
 - Lowers SO_x to ~ 1 ppmv from ~ 40 ppmv out of FGD
- Cansolv CO_2 Capture Process Details
 - 90 % CO_2 capture
 - Steam extraction from crossover pipe between IP and LP sections of steam turbine
 - Product $\text{CO}_2 \sim 30$ psia
- CO_2 Compression System
 - CO_2 compressed to 2,200 psig
 - 8 stages (2.23 to 1.48 stage pressure ratios)
 - Intercooling in each stage
 - Water knockout in first 3 stages
 - TEG dehydration unit between stages 4 and 5
 - 300 ppmw H_2O in CO_2 product



Advanced Stripper Alternative Process Configuration

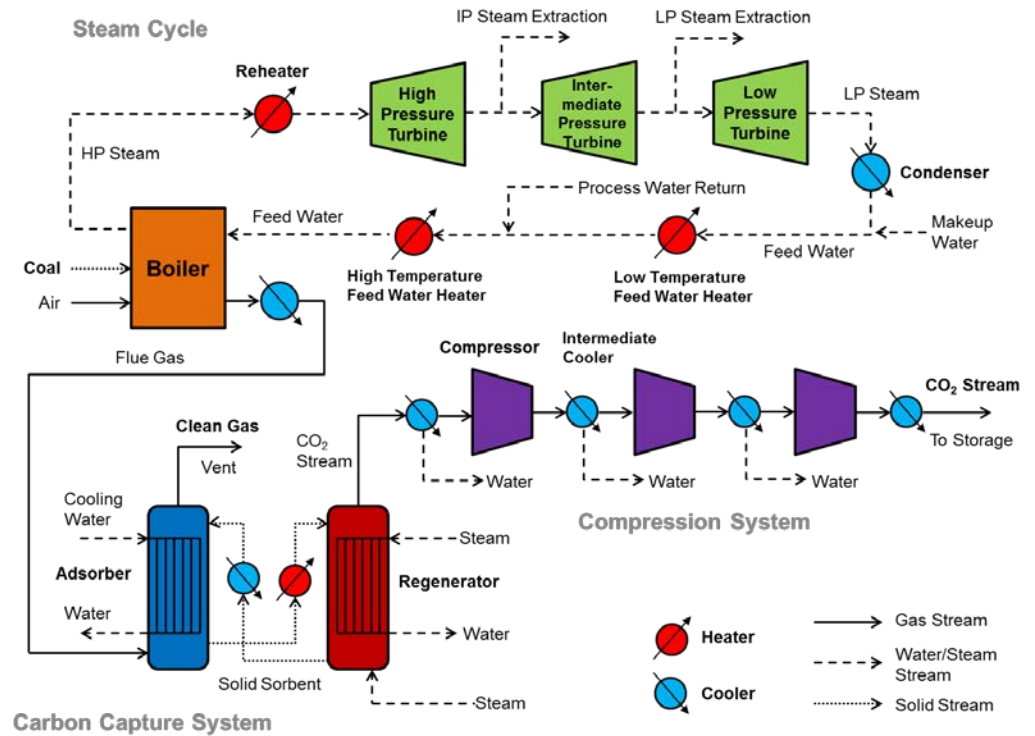


Optimization & Heat Integration

Objective: Max. Net efficiency

Constraint: CO₂ removal ratio ≥ 90%

Decision Variables (17): Bed length, diameter, sorbent and steam feed rate

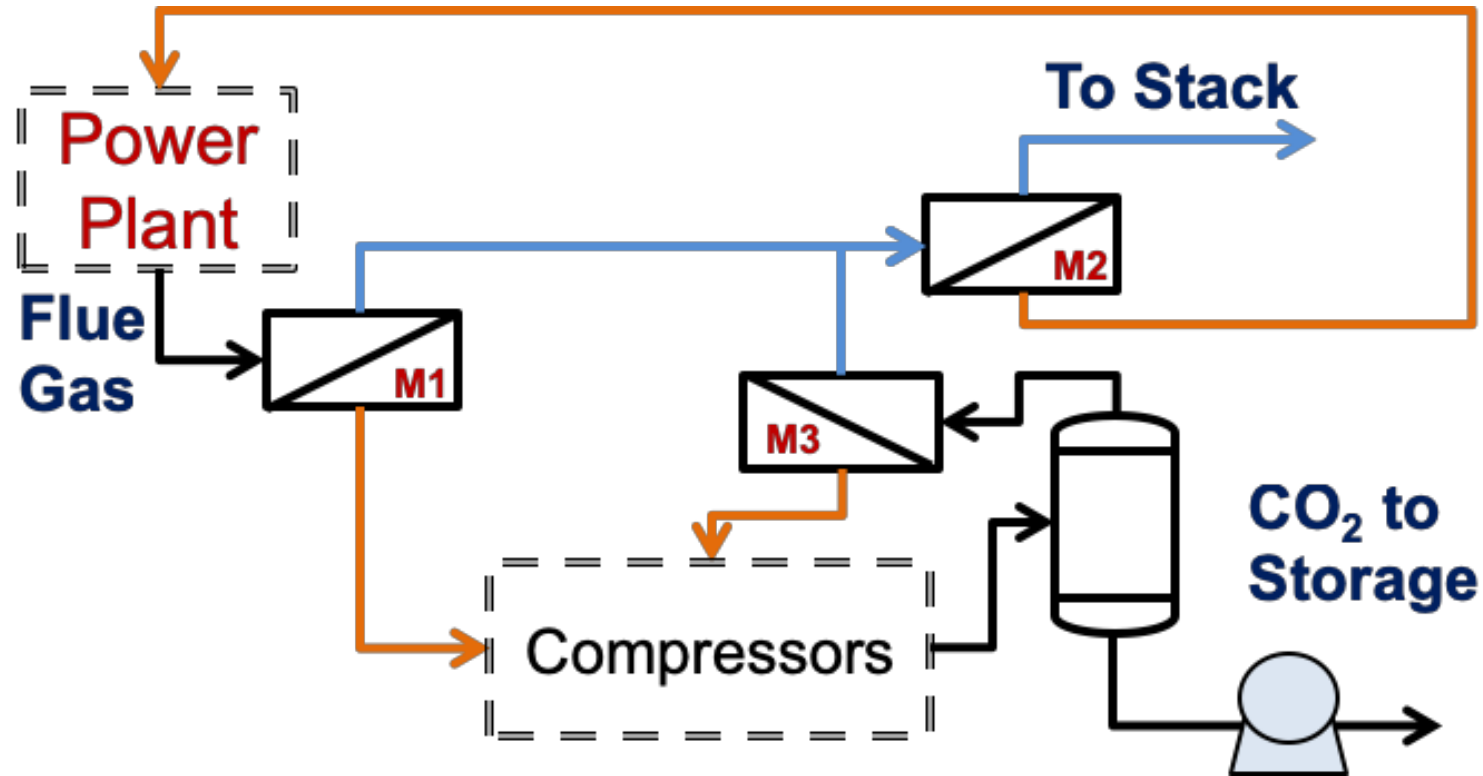


	w/o heat integration	Sequential	Simultaneous
Net power efficiency (%)	31.0	32.7	35.7
Net power output (MW _e)	479.7	505.4	552.4
Electricity consumption ^b (MW _e)	67.0	67.0	80.4

Base case w/o CCS: 650 MW_e, 42.1 %

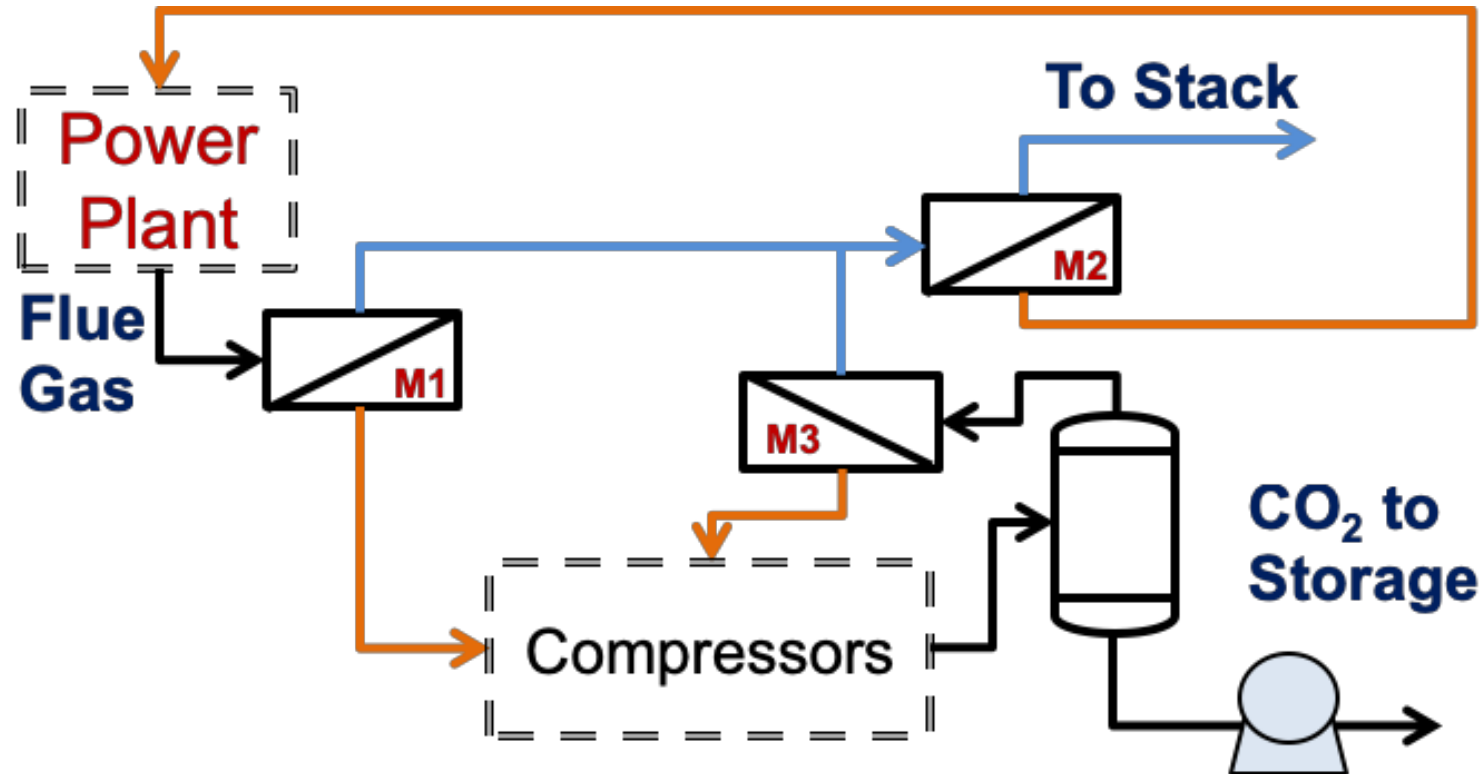
Simultaneous Optimization of Materials & Process

Membrane	Permeance (GPU)	Selectivity $\alpha_{\text{CO}_2/\text{N}_2}$	COE % Improvement	# Member Stages
Base	2500	28	Base	3



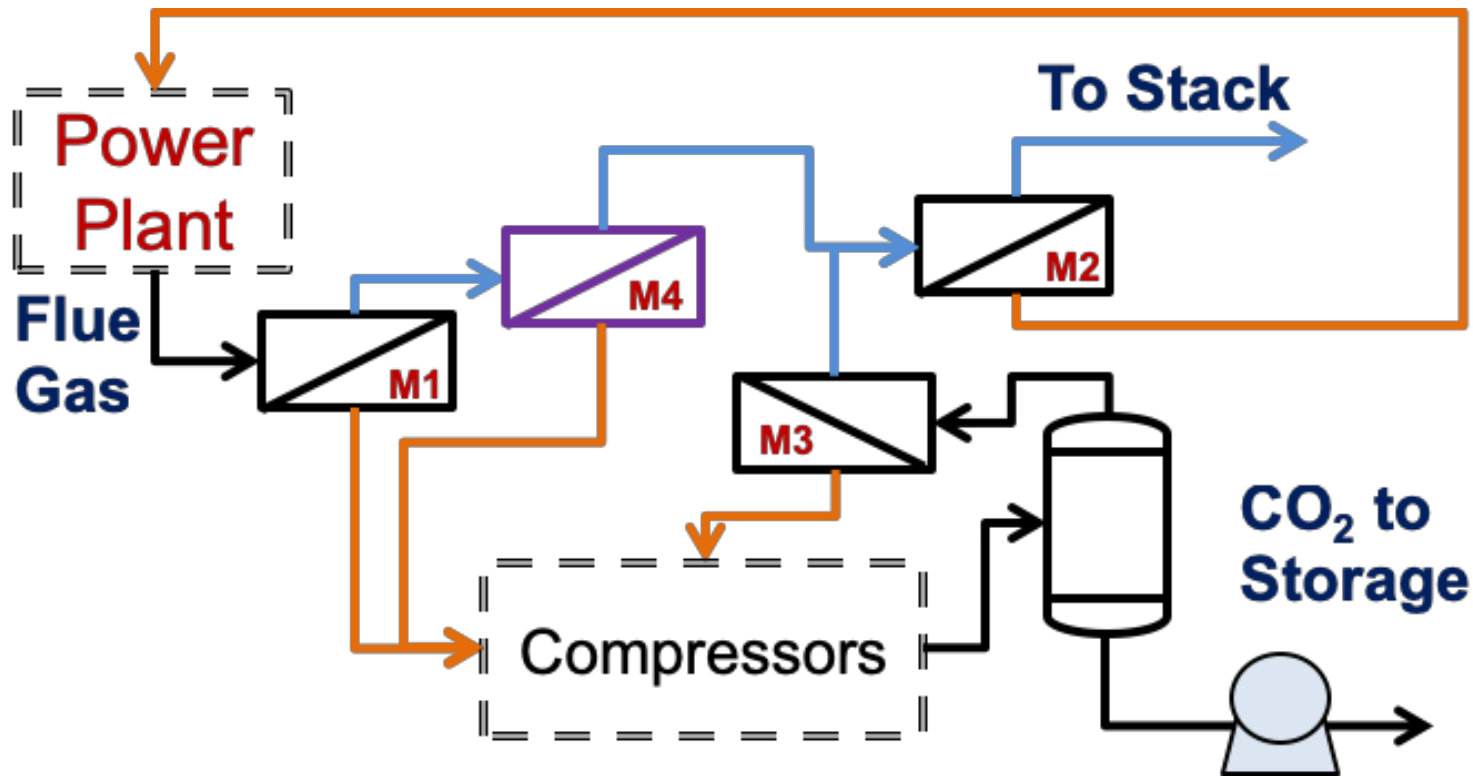
Simultaneous Optimization of Materials & Process

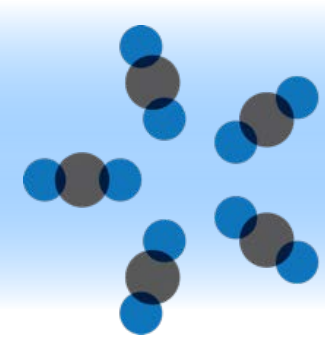
Membrane	Permeance (GPU)	Selectivity $\alpha_{\text{CO}_2/\text{N}_2}$	COE % Improvement	# Member Stages
Base	2500	28	Base	3
New	2600	74	9.5%	3



Simultaneous Optimization of Materials & Process

Membrane	Permeance (GPU)	Selectivity $\alpha_{\text{CO}_2/\text{N}_2}$	COE % Improvement	# Member Stages
Base	2500	28	Base	3
New	2600	74	9.5%	3
New	2600	74	14%	4





CCSI

Carbon Capture Simulation Initiative

Maximizing the learning at each stage of technology development

- **Early stage R&D**

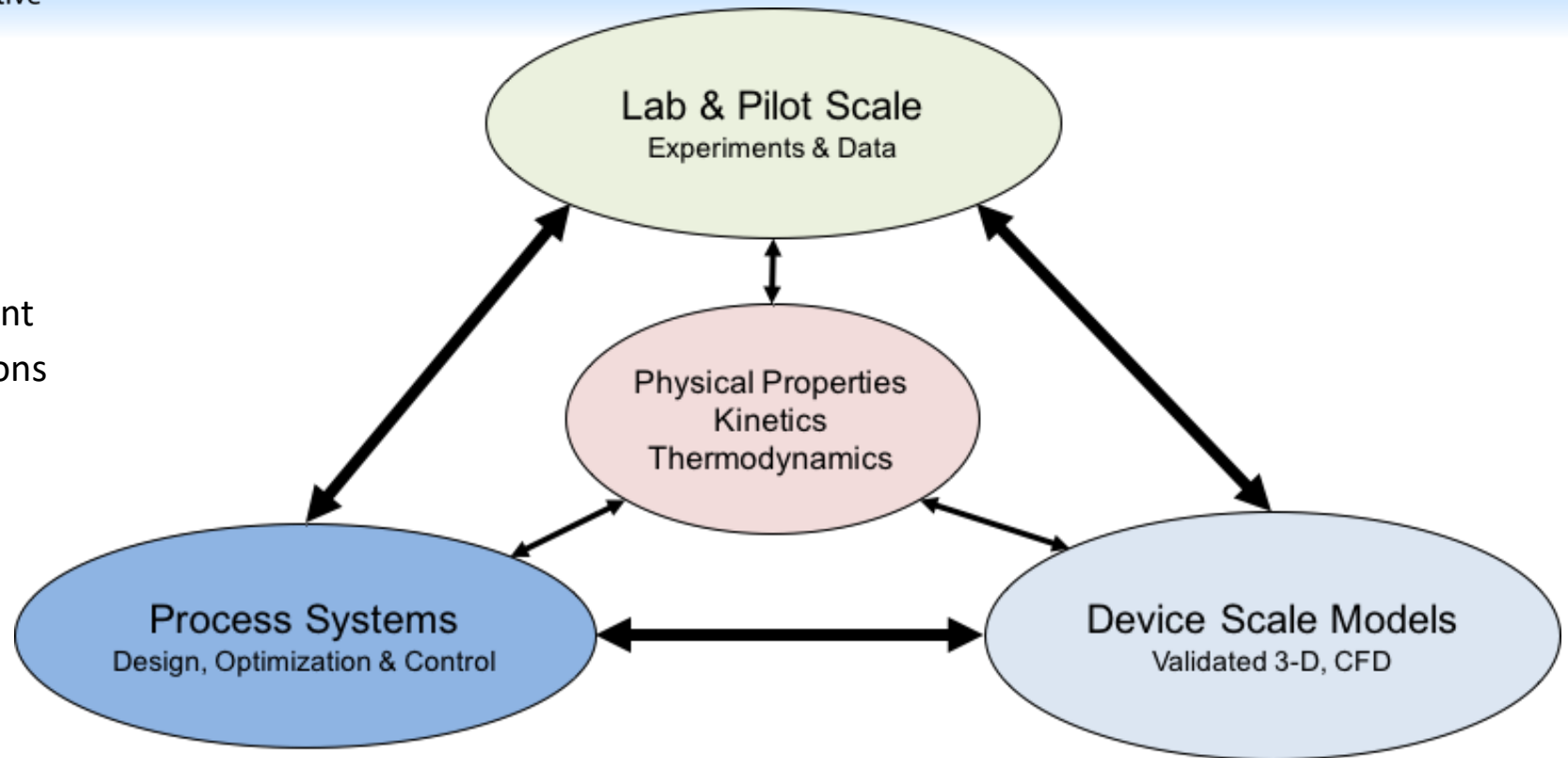
- Screening concepts
- Identify conditions to focus development
- Prioritize data collection & test conditions

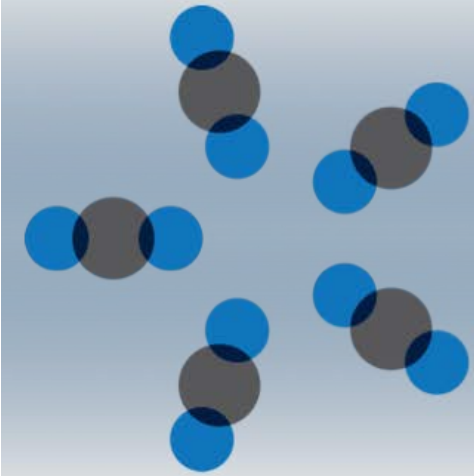
- **Pilot scale**

- Ensure the right data is collected
- Support scale-up design

- **Demo scale**

- Design the right process
- Support deployment with reduced risk





CCSI²

Carbon Capture Simulation for Industry Impact

Carbon Capture Pilot Plant Testing

Sequential Design of Experiments to Maximize Learning

Model + Experiments + Statistics

Ensure right data is collected
Maximize value of data collected

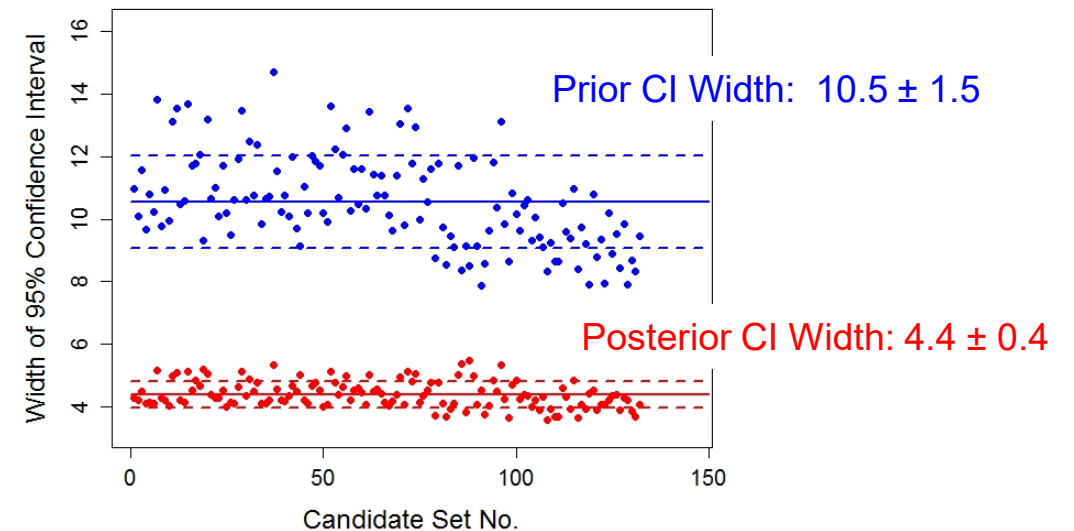
Early Stage Systems Design & Optimization

DOCCS Transformational Carbon Capture Projects

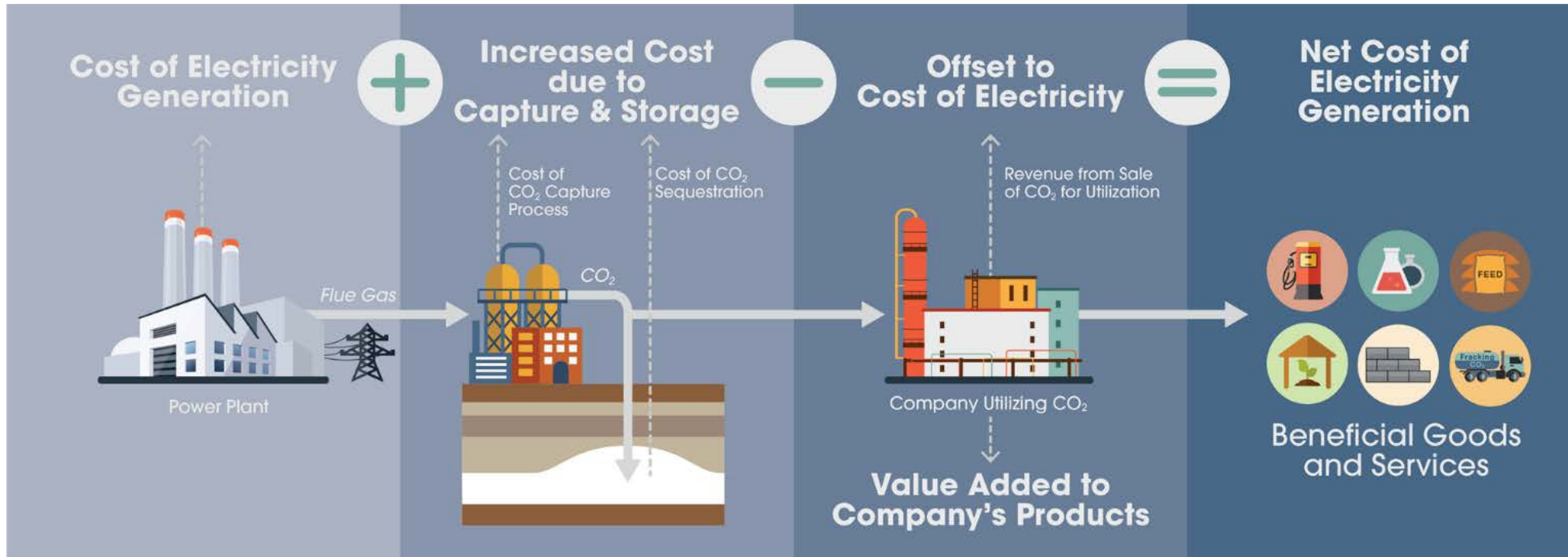


Technology Centre Mongstad – Summer 2018

www.tcmda.com

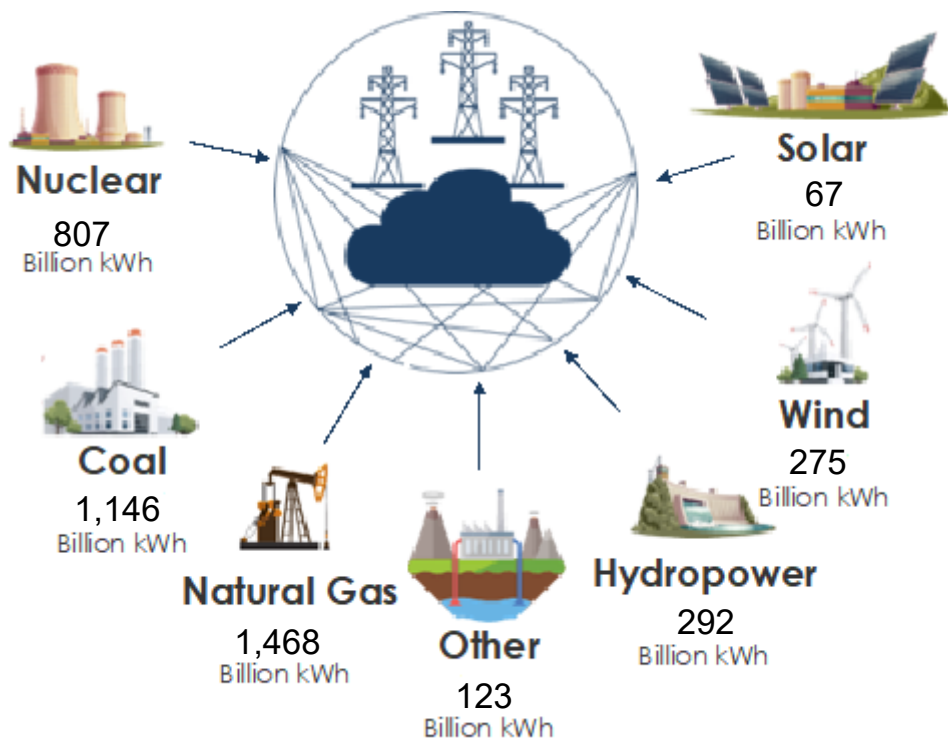


CO₂ Utilization Provides Revenue Stream



An Evolving Energy Ecosystem

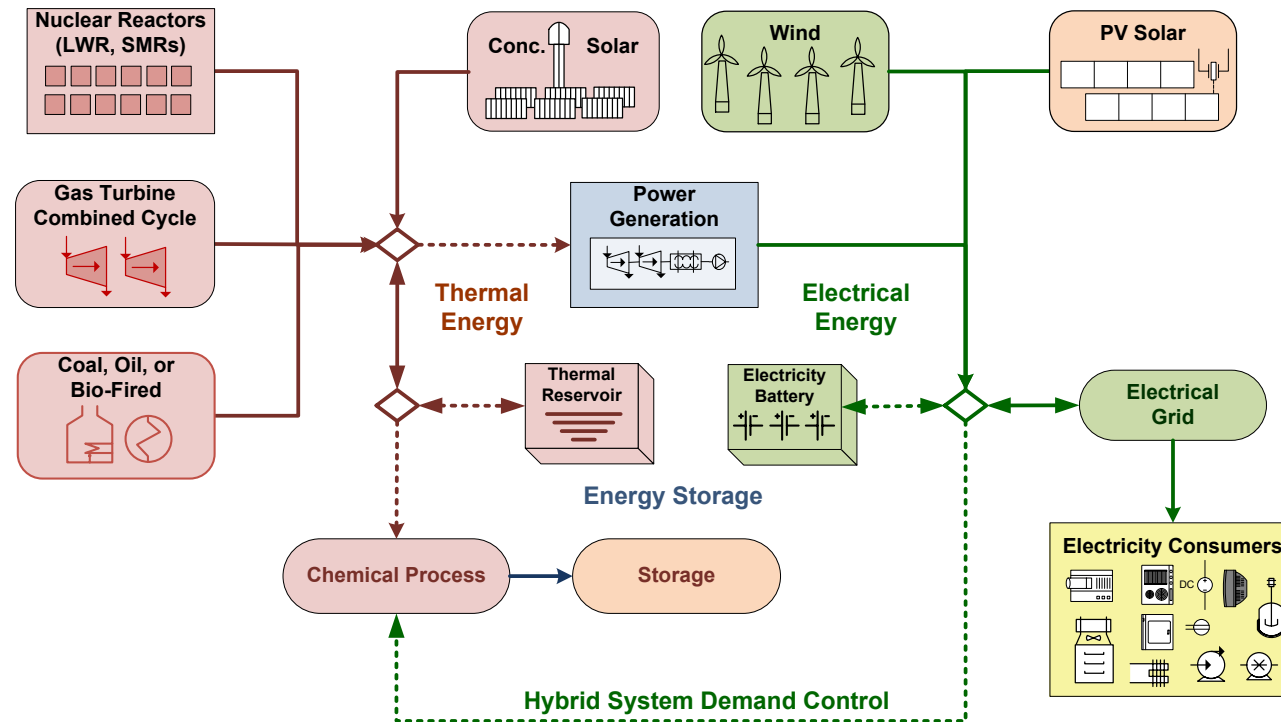
Coordinated Energy Systems



Total: 4,178 Billion kilowatt-hours (kWh)

Data source: EIA, 2018

Tightly Coupled Hybrid Energy Systems



Process Intensification & Modularization

- **Intensification** smaller, cleaner, and more energy-efficient technology
 - Reactive distillation
 - Dividing wall columns
 - Rotating packed bed
 - Microreactors
- **Modular design**
 - “Numbering up” instead of scaling up
 - Reduced investment risk
 - Improved time to market
 - Increased flexibility
 - Improved safety
 - Reduced on-site construction

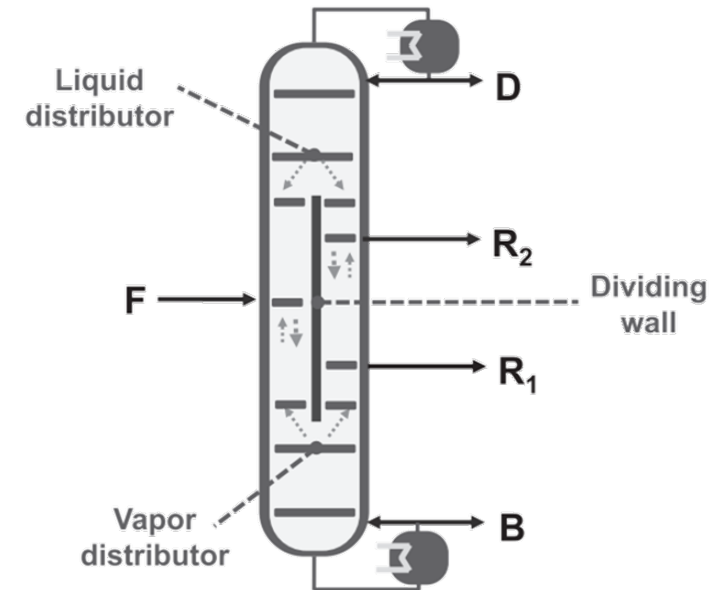
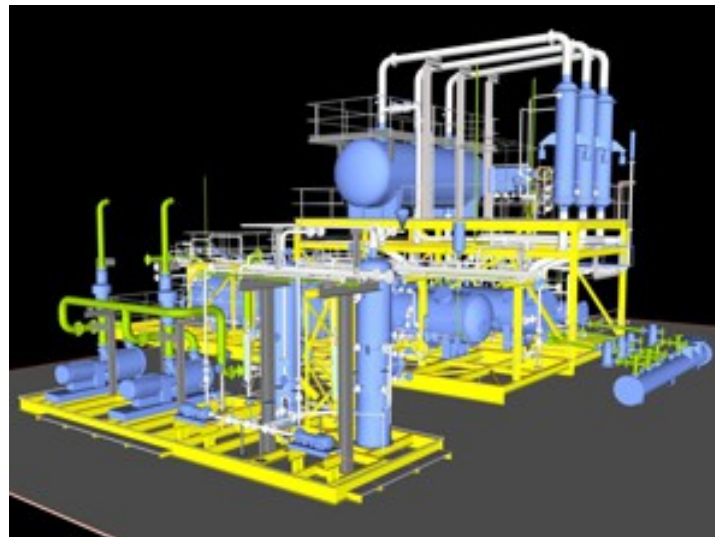
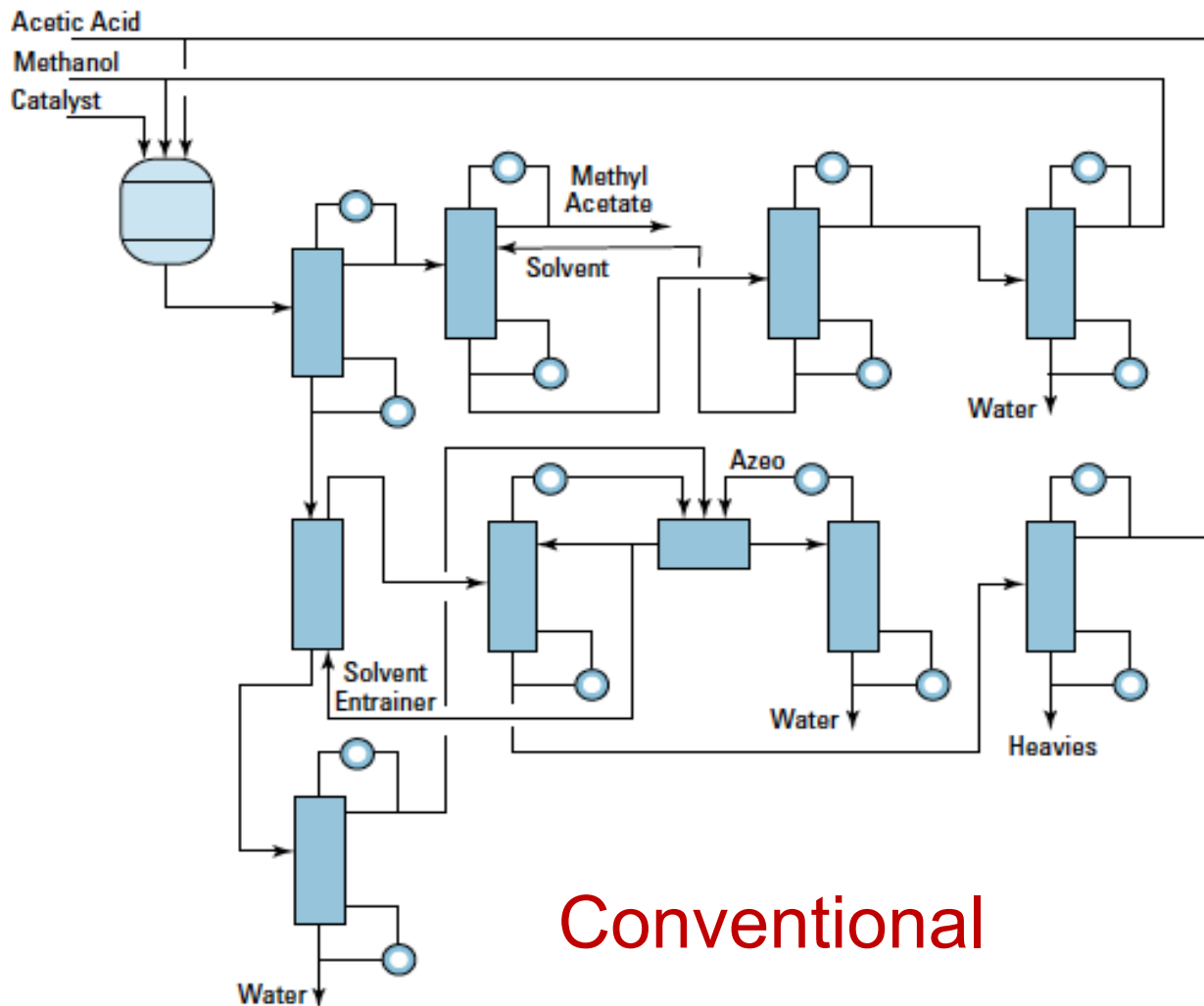


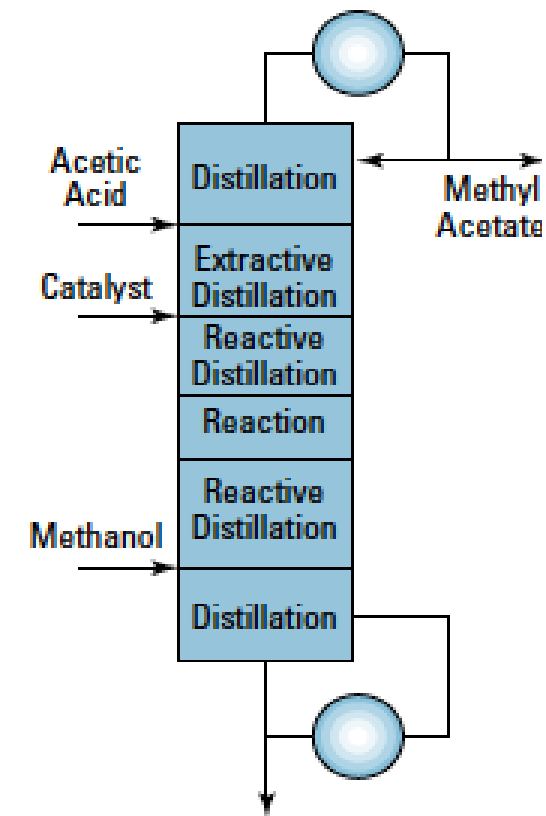
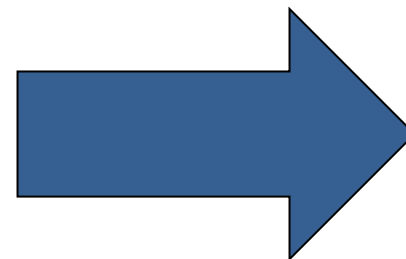
Figure from Rawlings et al., 2019



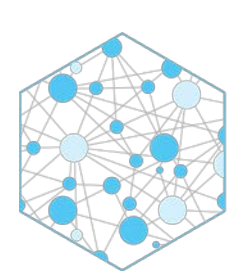
Process Intensification: Reactive Distillation



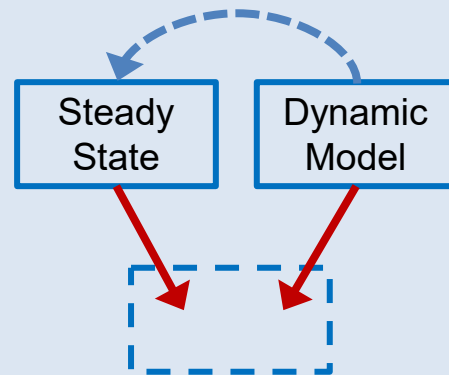
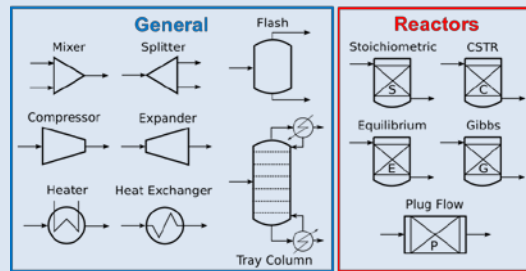
Conventional



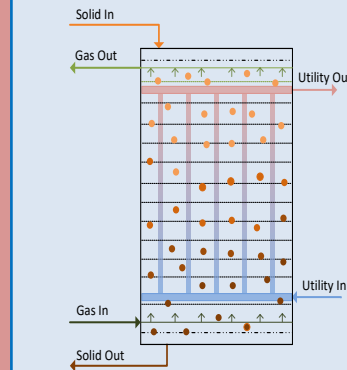
Integrated: 90% savings



Hierarchical Process Model Library

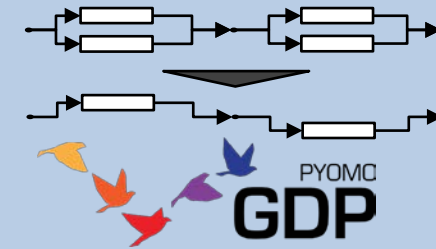


Model Customization

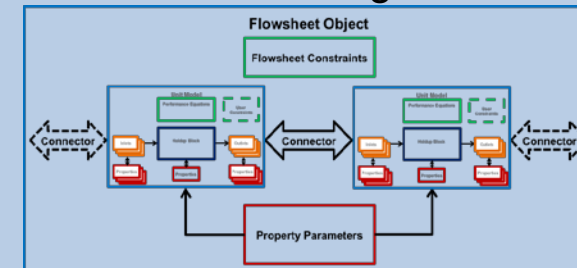


Algebraic Modeling Language

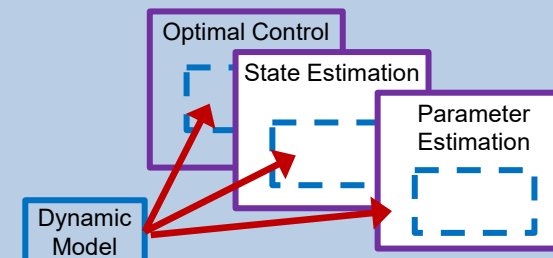
Conceptual Design via Superstructure



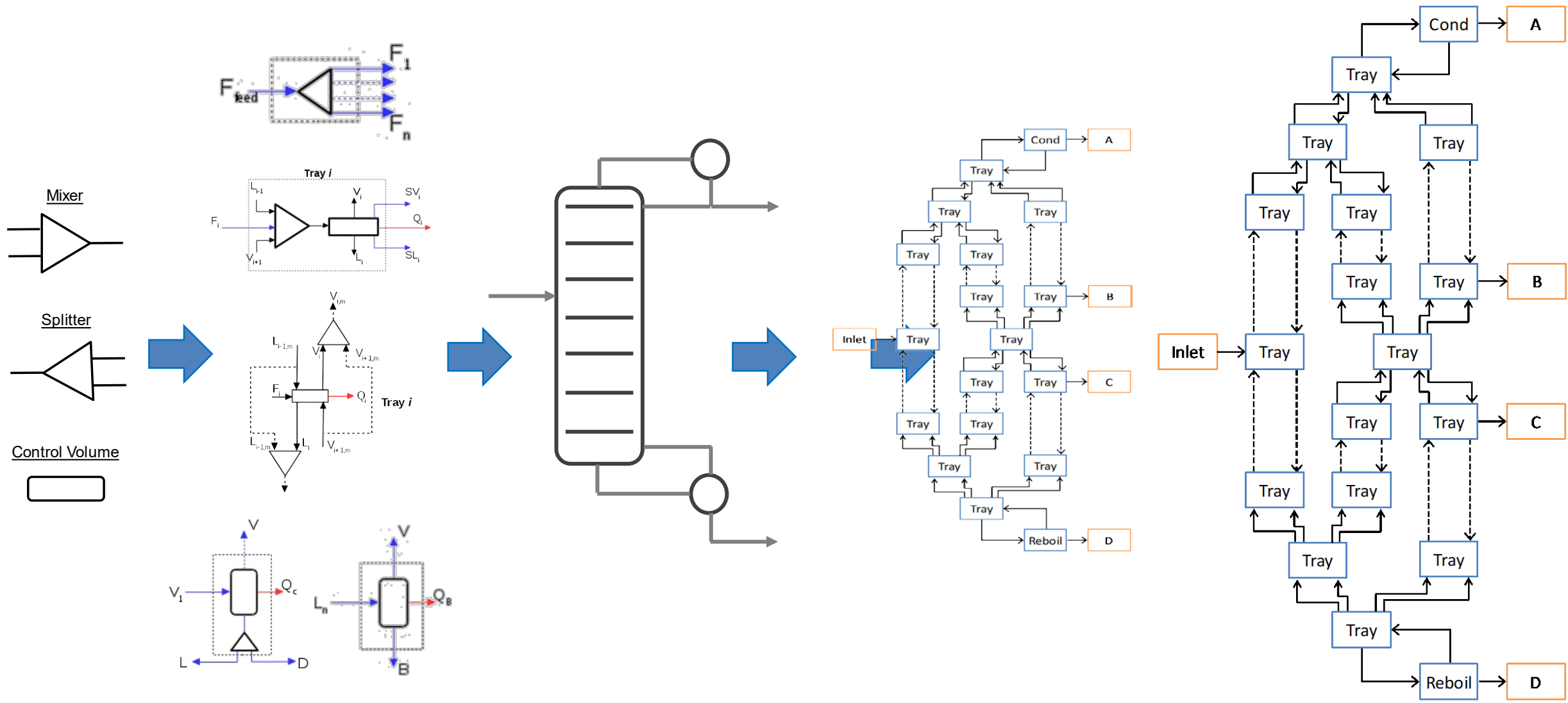
Process Design & Optimization Process Integration



Dynamics & Control

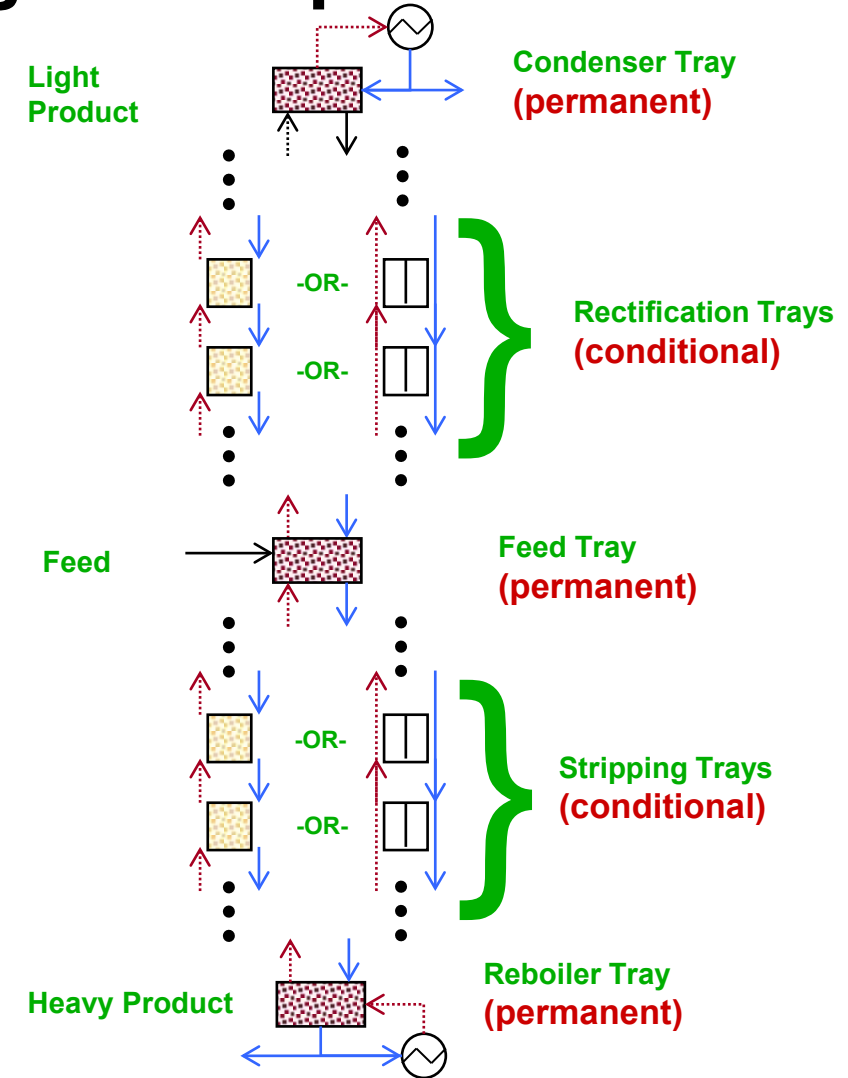
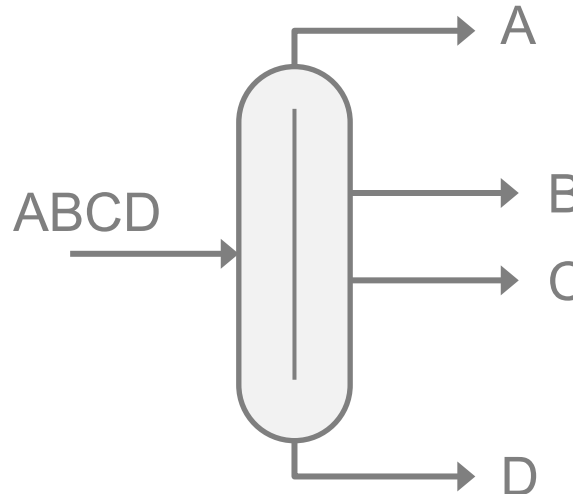


Basic blocks combine to model complex, intensified units



Kaibel Column Conceptual Design Example

- **Components:** Methanol, ethanol, n-propanol, n-butanol
 - 99% purity for each component
- **42 million combinations**
- **GDP model written using Pyomo.GDP**
 - 5715 constraints
 - 2124 nonlinear
 - 100 disjunctions
 - 3599 variables
 - 178 binary
 - 3421 continuous
- **Solved in 639 sec using GDPopt-LOA solver**
 - Logic-based outer approximation algorithm
 - **4 iterations**
- **Resulting design:**
 - **46 trays** (21% reduction vs. base case)
 - **Dividing wall between 12th and 26th tray**
 - **Feed at 18th tray**
 - **Side outlets at 13th and 22nd trays**



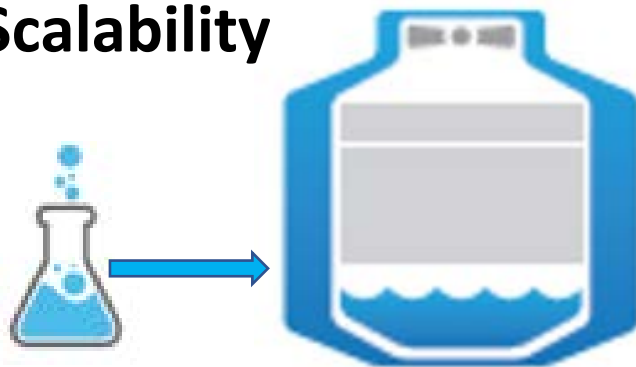
Optimal Design Kaibel Column reduces energy consumption by more than 40% compared to 2 columns

Challenges & Opportunities

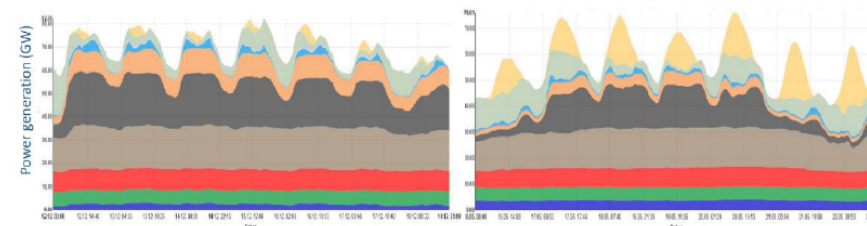
Market Risk



Scalability



Variability of CO₂ streams

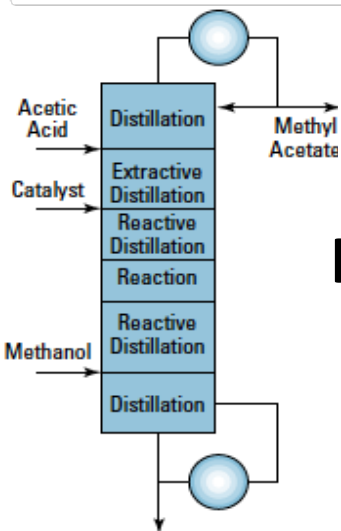


Technology Stability with Contaminants

NO_x SO_x
trace elements



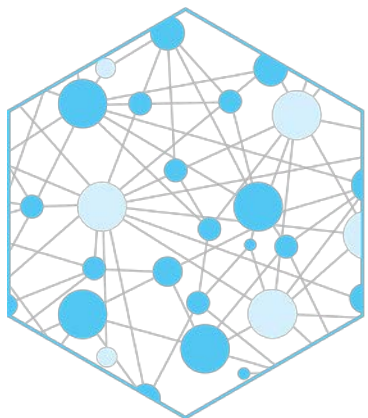
Process Intensification System Development



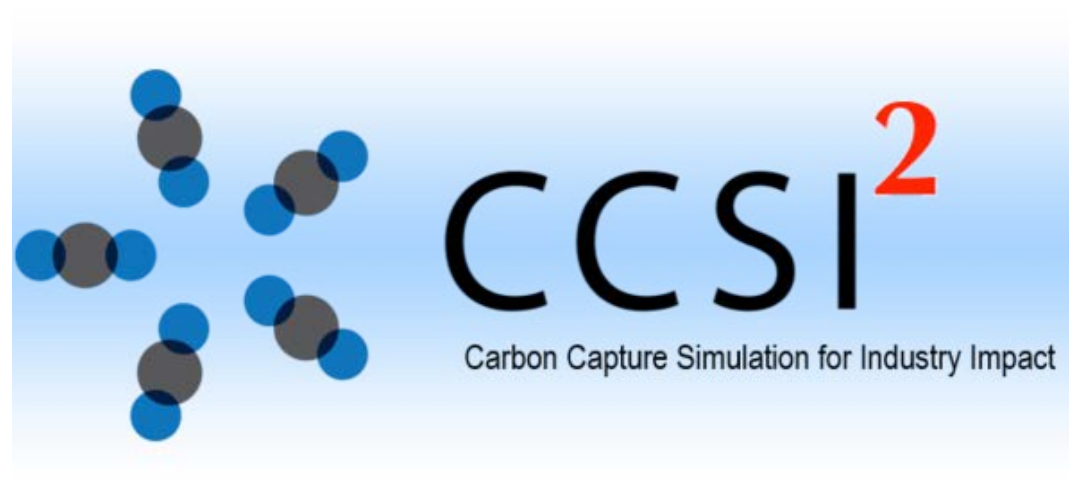
Life Cycle Analysis

Conclusion

- Economics & Viability are f (system)
- Optimal system = f (materials, technology, concentration, operational approach)



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